SMNSR-U0-000818-2016 001

Chipeta Processing LLC P.O. Box 173779, Denver, Colorado 80217-3779 720-929-6000 Fax 720-929-7000

RECEIVED NOV 0 8 2016

November 4, 2016

SENT VIA CERTIFIED MAIL No.:

7014 2120 0003 6311 0650

Ms. Claudia Smith U.S. EPA, Region 8 1595 Wynkoop Street, 8P-AR Denver, CO 80202-1129

RE: Synthetic Minor NSR Permit Application under Part 49

Bitter Creek Compressor Station

Dear Ms. Smith:

Anadarko Uintah Midstream, LLC (Anadarko) is submitting the attached permit application under Part 49 Minor NSR rules for the Bitter Creek Compressor Station located in Uintah County, Utah. Anadarko is submitting this minor source application to establish federally enforceable limits as required by the Civil Action No. 07-CV-01034-EWN-KMT (KMG Consent Decree).

The attached application contains the following:

Appendix A: EPA Form New

Appendix B: EPA Form SYNMIN

Appendix C: Process Description, Flow Diagram, and Plot Plan Appendix D: Emission Unit and Emission Control Descriptions

Appendix E: Emission Summary

Appendix F: Detailed Emission Calculations

Appendix G: Regulatory Analysis

Sincerely,

Anadarko Lintah Midstream, LLC

Natalie Ohlhausen

Sr. HSE Representative

Enclosures

Appendix A

Form NEW

(Application for New Construction)

OMB Control No. 2060-0003 Approval expires 04/30/2012



United States Environmental Protection Agency Program Address Phone Fax Web address

Reviewing Authority Program Address Phone Fax Web address

FEDERAL MINOR NEW SOURCE REVIEW PROGRAM IN INDIAN COUNTRY

Application for New Construction

| (Form NEW) |
|---|
| Please check all that apply to show how you are using this form: |
| ☐ Proposed Construction of a New Source |
| ☐ Proposed Construction of New Equipment at an Existing Source |
| ☐ Proposed Modification of an Existing Source |
| ☑ Other – Please Explain |
| Existing Source operating under synthetic minor limits, as regulated |
| under Consent Decree, submitting an application for a synthetic minor |
| permit under Part 49. |

Please submit information to:

Ms. Claudia Smith U.S. EPA Region 8 1595 Wynkoop Street, 8P-AR Denver, CO 80202-1129

A. GENERAL SOURCE INFORMATION

| 1. (a) Company Name | | 2. Source Name | | |
|--|-----------------------|--|-----------------|--|
| Anadarko Uintah | Midstream LLC | Bitter Creek Comp | ressor Station | |
| (b) Operator Name | | | | |
| Anadarko Uintah | Midstream LLC | | | |
| 3. Type of Operation Nat.Gas Compression | & Transmission | 4. Portable Source? ☐ 5. Temporary Source? ☐ | | |
| 6. NAICS Code | | 7. SIC Code 1311 | | |
| 8. Physical Address (home base | for portable sources) | | | |
| 9. Reservation* | 10. County* | 11a. Latitude* | 11b. Longitude* | |
| Uintah and Ouray | Uintah | 39.934358° N | -109.48531 ° W | |
| 12a. Quarter Quarter Section* | 12b. Section* | 12c. Township* | 12d. Range* | |
| NE SW | 19 | 10S | 22E | |

^{*}Provide all proposed locations of operation for portable sources

| B. PREVIOUS PERMIT ACTIONS (Provide information in this format for each permit that has |
|---|
| been issued to this source. Provide as an attachment if additional space is necessary) |
| Source Name on the Permit |
| |
| Permit Number (xx-xxx-xxxxx-xxxxxxx) |
| |
| |
| Date of the Permit Action |
| |
| |
| Source Name on the Permit |
| |
| |
| Permit Number (xx-xxx-xxxxx-xxxxxxx) |
| |
| Date of the Permit Action |
| |
| |
| |
| Source Name on the Permit |
| |
| Permit Number (xx-xxx-xxxxx-xxxx.xx) |
| |
| |
| Date of the Permit Action |
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| |
| Source Name on the Permit |
| Source Name on the Fermit |
| |
| Permit Number (xx-xxx-xxxx-xxxxxxxxxxxxxxxxxxxxxxxxx |
| |
| Date of the Permit Action |
| Date of the Fernit Action |
| |
| |
| Source Name on the Permit |
| |
| Permit Number (xx-xxx-xxxxx-xxxx.xx) |
| 1 CHILL HULLIOOL (AATAAATAAAATAAA) |
| |
| Date of the Permit Action |
| |

C. CONTACT INFORMATION

| Company Contact | Title | |
|--|------------------|------------------------|
| Mike Weaver | Midstre | am Operations Manager |
| Mailing Address P.O.Box 173779, Denver, CO 80202- | 3779 | |
| Email Address Mike.Weaver@anadarko.com | | |
| Telephone Number 720-929-6792 | Facsimile Number | |
| Operator Contact (if different from company contact) Andy Zeller | | Title Plant Foreman |
| Mailing Address | | |
| Email Address andy.zeller@anadarko.com | | |
| | Farainila Nivela | |
| Telephone Number 435-781-7001 | Facsimile Number | |
| Source Contact | | Title |
| Natalie Ohlhausen | | Sr. HSE Representative |
| Mailing Address | | |
| P.O.Box 173779, Denver, CO 80202-3 | 3779 | |
| Email Address | | |
| Natalie.Ohlhausen@Anadarko.com | | |
| Telephone Number | Facsimile Number | ALC: |
| 720-929-6498 | | |
| Compliance Contact | Title | |
| Same as Source Contact | | |
| Mailing Address | | |
| Email Address | | |
| Telephone Number | Facsimile Number | |
| | | |

D. ATTACHMENTS

Include all of the following information (see the attached instructions)

M FORM SYNMIN - New Source Review Synthetic Minor Limit Request Form, if synthetic minor limits are being requested. \(\times\) Narrative description of the proposed production processes. This description should follow the flow of the process flow diagram to be submitted with this application. ☑ Process flow chart identifying all proposed processing, combustion, handling, storage, and emission control equipment. ☑ A list and descriptions of all proposed emission units and air pollution-generating activities. \(\times\) Type and quantity of fuels, including sulfur content of fuels, proposed to be used on a daily, annual and maximum hourly basis. ☑ Type and quantity of raw materials used or final product produced proposed to be used on a daily, annual and maximum hourly basis. \(\times\) Proposed operating schedule, including number of hours per day, number of days per week and number of weeks per year. A list and description of all proposed emission controls, control efficiencies, emission limits, and monitoring for each emission unit and air pollution generating activity. M Criteria Pollutant Emissions - Estimates of Current Actual Emissions, Current Allowable Emissions, Post-Change Uncontrolled Emissions, and Post-Change Allowable Emissions for the following air pollutants: particulate matter, PM₁₀, PM_{2.5}, sulfur oxides (SOx), nitrogen oxides (NOx), carbon monoxide (CO), volatile organic compound (VOC), lead (Pb) and lead compounds, fluorides (gaseous and particulate), sulfuric acid mist (H₂SO₄), hydrogen sulfide (H₂S), total reduced sulfur (TRS) and reduced sulfur compounds, including all calculations for the estimates. These estimates are to be made for each emission unit, emission generating activity, and the project/source in total.

☐ Modeling – Air Quality Impact Analysis (AQIA)

□ NHPA (National Historic Preservation Act)

☐ ESA (Endangered Species Act)

E. TABLE OF ESTIMATED EMISSIONS

The following tables provide the total emissions in tons/year for all pollutants from the calculations required in Section D of this form, as appropriate for the use specified at the top of the form.

E(i) - Proposed New Source

| Pollutant | Potential Emissions (tpy) | Proposed Allowable Emissions (tpy) | |
|--------------------------------|------------------------------|--|--|
| PM | | 0.0 | PM - Particulate Matter PM ₁₀ - Particulate Matter less |
| PM ₁₀ | | 0.0 | than 10 microns in size |
| PM _{2.5} | | 0.0 | PM _{2.5} - Particulate Matter less than 2.5 microns in size |
| SO _x | | | SOx - Sulfur Oxides NOx - Nitrogen Oxides |
| NO _x | | 39.1 | CO - Carbon Monoxide |
| СО | | 15.6 | VOC - Volatile Organic Compound |
| VOC | | 23.5 | Pb - Lead and lead compounds Fluorides - Gaseous and |
| Pb | | | particulates |
| CO2e | | 12044.8 | H ₂ SO ₄ - Sulfuric Acid Mist H ₂ S - Hydrogen Sulfide |
| Fluorides | | | TRS - Total Reduced Sulfur |
| H ₂ SO ₄ | | | RSC - Reduced Sulfur Compounds |
| H ₂ S | | | Compounds |
| TRS | | | |
| RSC | | | 1 |

Emissions calculations must include fugitive emissions if the source is one the following listed sources, pursuant to CAA Section 302(j):

- (a) Coal cleaning plants (with thermal dryers);
- (b) Kraft pulp mills;
- (c) Portland cement plants;
- (d) Primary zinc smelters;
- (e) Iron and steel mills;
- (f) Primary aluminum ore reduction plants;
- (g) Primary copper smelters;
- (h) Municipal incinerators capable of charging more than 250 tons of refuse per day;
- (i) Hydrofluoric, sulfuric, or nitric acid plants;
- (j) Petroleum refineries;
- (k) Lime plants;
- (1) Phosphate rock processing plants;
- (m) Coke oven batteries;
- (n) Sulfur recovery plants;
- (o) Carbon black plants (furnace process);
- (p) Primary lead smelters;
- (q) Fuel conversion plants;

- (r) Sintering plants;
- (s) Secondary metal production plants;
- (t) Chemical process plants
- (u) Fossil-fuel boilers (or combination thereof) totaling more than 250 million British thermal units per hour heat input;
- (v) Petroleum storage and transfer units with a total storage capacity exceeding 300,000 barrels;
- (w) Taconite ore processing plants;
- (x) Glass fiber processing plants;
- (y) Charcoal production plants;
- (z) Fossil fuel-fired steam electric plants of more that 250 million British thermal units per hour heat input, and
- (aa) Any other stationary source category which, as of August 7, 1980, is being regulated under section 111 or 112 of the Act.

Appendix B

Form SYNMIN

(Application for Synthetic Minor Limit)



United States Environmental Protection Agency **Program** Address Phone Fax

Reviewing Authority Program Address Phone Fax Web address

FEDERAL MINOR NEW SOURCE REVIEW PROGRAM IN INDIAN COUNTRY

Web address

Application For Synthetic Minor Limit

(Form SYNMIN)

Please submit information to:

Ms. Claudia Smith U.S. EPA Region 8 Air and Toxics Division 1595 Wynkoop Denver, CO 80202-1129

A. GENERAL INFORMATION

| Company Name Anadarko Uintah Midstream LLC | Source Name Bitter Creek Compressor Station |
|---|---|
| Company Contact or Owner Name Mike Weaver | Title Midstream Operations Manager |
| Mailing Address P.O.Box 173779, Denver, CO 80202-3 | 779 |
| Email Address Mike.Weaver@anadarko.com | |
| Telephone Number | Facsimile Number |
| 720-929-6792 | |

B. ATTACHMENTS For each criteria air pollutant, hazardous air pollutant and for all emission units and air pollutantgenerating activities to be covered by a limitation, include the following: ☑ Item 1 - The proposed limitation and a description of its effect on current actual, allowable and the potential to emit. ☑ Item 2 - The proposed testing, monitoring, recordkeeping, and reporting requirements to be used to demonstrate and assure compliance with the proposed limitation. ☑ Item 3 - A description of estimated efficiency of air pollution control equipment under present or anticipated operating conditions, including documentation of the manufacturer specifications and guarantees. ☑ Item 4 - Estimates of the Post-Change Allowable Emissions that would result from compliance with the proposed limitation, including all calculations for the estimates.

☑ Item 5 – Estimates of the potential emissions of Greenhouse Gas (GHG) pollutants:

Appendix C

Process Description, Process Flow Diagram, & Plot Plan

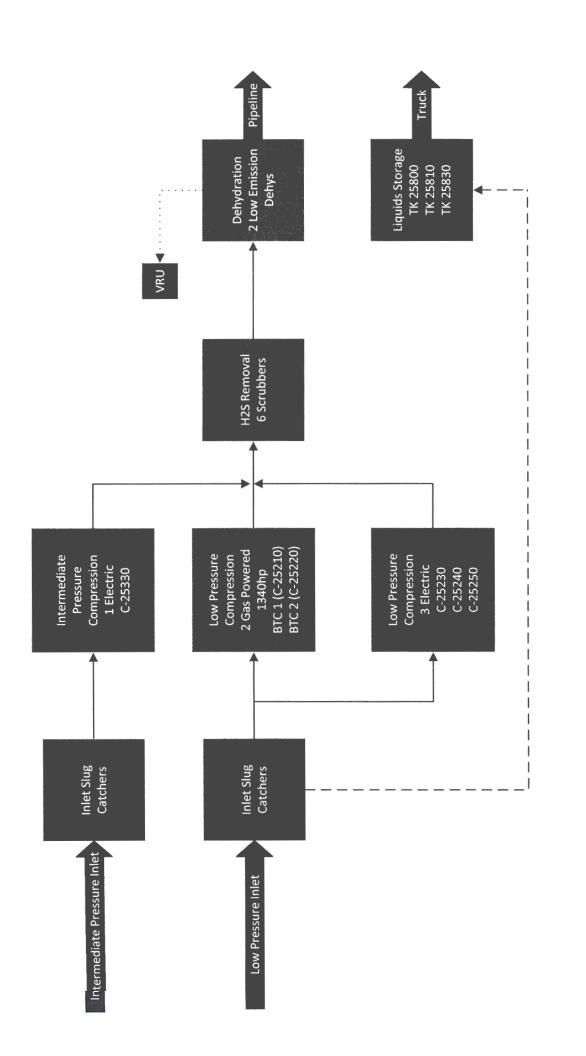
Process Description

Anadarko Uintah Midstream LLC (Anadarko) owns and operates the Bitter Creek Compressor Station (Bitter Creek), within the exterior boundaries of the Uintah and Ouray Indian Reservation, in Uintah County, Utah.

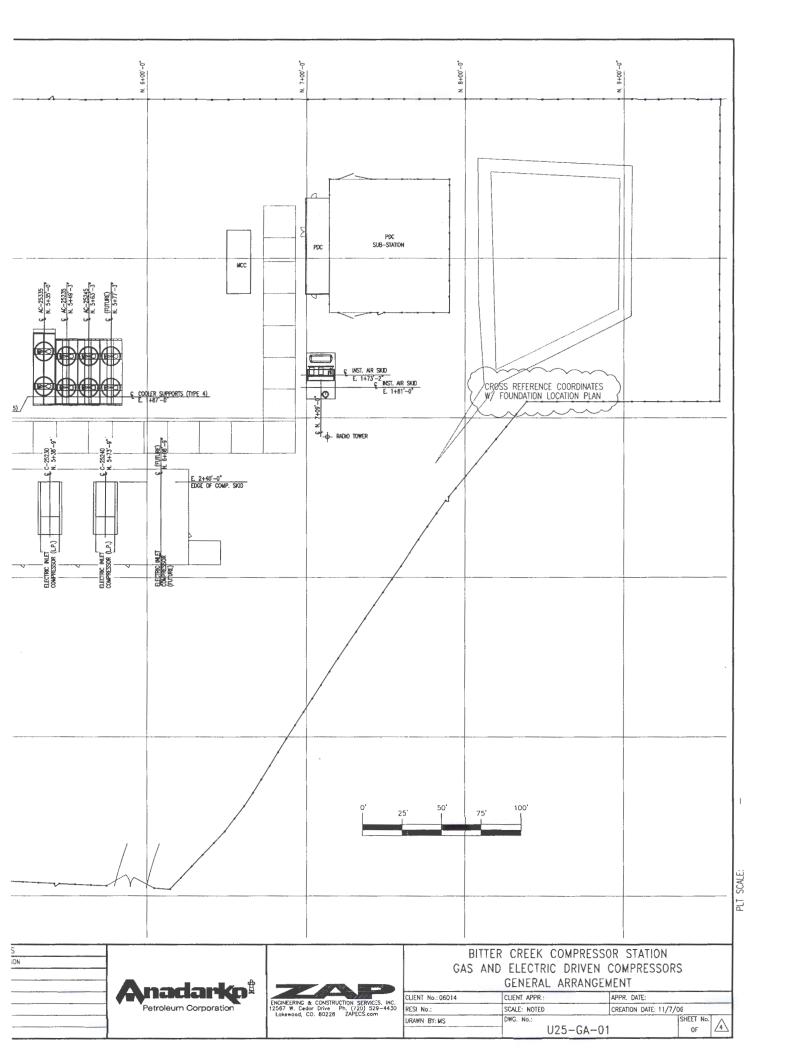
Natural gas from the surrounding field is routed to the compressor station via the gas collection system. Natural gas enters the compressor station through the inlet slug catchers where liquids are gravitationally separated from the stream. Condensate recovered is sent to the blowcase system and put back into the discharge line leaving the station. Gas goes through two stages of compression before discharge from the facility. Water is stored in the atmospheric storage tanks along with condensate collected. Liquids are held in storage tanks onsite until loaded into trucks for transport to sale.

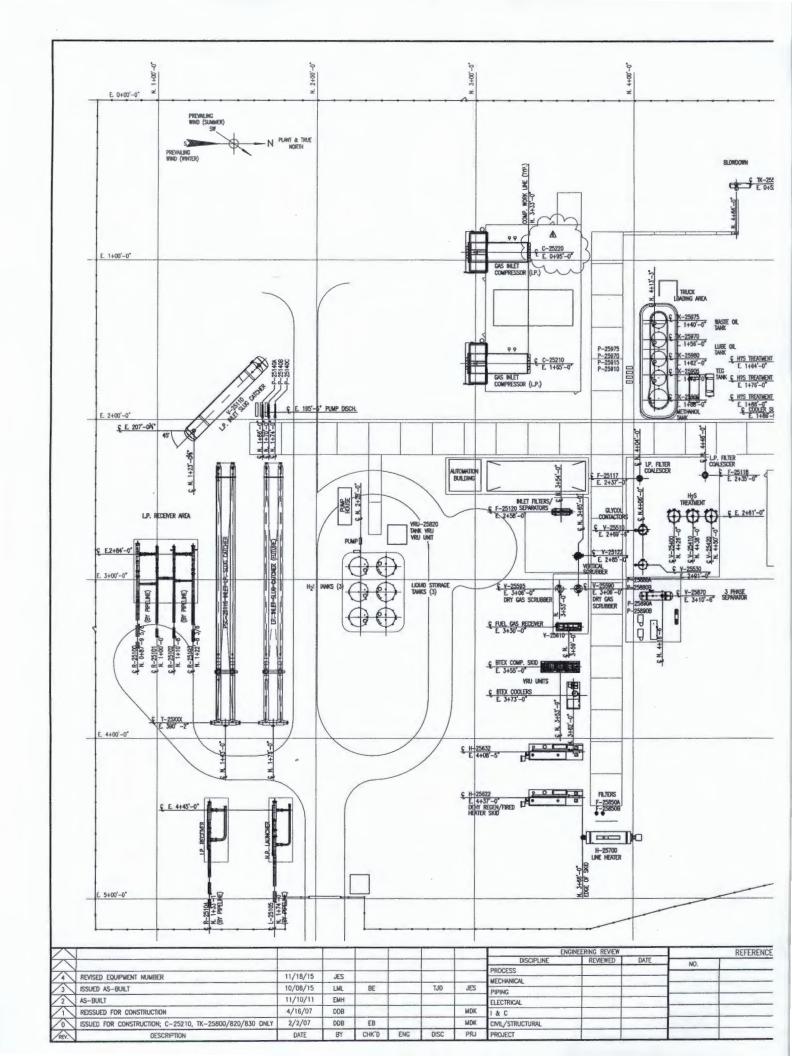
Bitter Creek operations consists of:

- Two Caterpillar G3516 compressor engines (BTC 1 and BTC 2),
- Two low emission dehydration units (DEHY-1 and 2)
- Three produced water tanks (Tank-25800, 25810, 25830)
- One truck loading area
- One 0.5 MMBtu/hr line heater (HTR-1)
- Two <0.01 MMBtu/hr dehydration unit reboilers (HTR-1 and 3)
- Piping components (FUG)



Bitter Creek Compressor Station Block Flow Diagram October 2016





Appendix D

Emission Unit Description

CO Emissions:

As per the Kerr-McGee ("KMG") Consent Decree, KMG is requesting to make the emission limits outlined in paragraphs 41 and 50 federal enforceable as required by paragraph 167. All engines located at the Bitter Creek Compressor Station are fitted with oxidation catalyst which demonstrate a control efficiency of 93% is required for these RICEs as per the Kerr-McGee Consent Decree (paragraphs 41 and 50).

KMG is requesting the control requirements for CO in the Consent Decrees be incorporated as permit conditions.

Proposed limits

CO emission control efficiency of 93% for Engines BTC 1 (C-25210) and BTC 2 (C-25210)

- Proposed testing
 - Initial Testing
 - Swap-outs and Like-kind Replacement Engines
 - Initial compliance test shall be conducted within 60 days after achieving the maximum production rate at which the affected facility will be operated, but not later than 180 days after initial startup.

Test Methods:

- Measure the O₂ and CO at the outlet of the control device using portable analyzer. Use ASTM D6522-00 (2005), Method 10 of 40 CFR appendix A, or some other EPA approved Method for CO.
 Measurements to determine O₂ must be made at the same time as the measurements for CO concentration.
- Convert to g/hp-hr using Method 19 and the manufacturer's specific fuel consumption or measured fuel consumption and horsepower at the time of the testing.
- Conduct one (1) test run for each performance test required. Each test run must last at least 21 minutes

• Ongoing Testing

Semi-annual or annual testing must be completed to verify compliance with g/hp-hr limits. Existing engines currently follow a semi-annual testing schedule. After permit issuance, if there is documented history of two consecutive, passing compliance tests, the testing frequency shall be reduced to annually. Overall, the testing frequency will not be reduced to annual tests until there are two consecutive, passing compliance tests (taking into account pre-permit, compliant tests). Total facility CO emissions shall be calculated based on the results of the latest test and 8,760 hours per year of operation. Should there

be a failed test, testing will resort to semi-annual testing. Two compliant semi-annual tests will be required before reverting to annual testing. Semi-annual tests must be completed within 180 days of permit issuance and annual tests must be completed within 365 days of permit issuance. Subsequent semi-annual and annual tests must occur anytime within the January to June and July to December semi-annual period or calendar year period, for semi-annual and annual testing, respectively. This means there will be instances where the time in between semi-annual tests may exceed 180 days and the time in between annual tests may exceed 365 days.

Test Methods:

- Measure the O₂ and CO at the outlet of the control device using portable analyzer. Use ASTM D6522-00 (2005), Method 10 of 40 CFR appendix A, or some other EPA approved Method for CO.
 Measurements to determine O₂ must be made at the same time as the measurements for CO concentration.
- Convert to g/hp-hr using Method 19 and the manufacturer's specific fuel consumption or measured fuel consumption and horsepower at the time of the testing.
- Conduct one (1) test run for each performance test required. Each test run must last at least 21 minutes

• Reporting Requirements

- Notification of performance test shall be submitted 30 days prior to the date of the performance test.
- Test reports shall be submitted within 60 days of completion of any compliance test.

Operation and Maintenance Requirements

 At all times, the permittee must operate and maintain any affected source, including associated air pollution control equipment and monitoring equipment, in a manner consistent with safety and good air pollution control practices for minimizing emissions.

Formaldehyde Emissions:

 This facility is a not major source of HAPs and is therefore not subject to the major source requirements of NESHAP Subpart ZZZZ. Therefore, no limits are being requested.

NOx Emissions:

• This facility NOx emissions are below the PSD threshold and, therefore, no limits are being requested.

VOC Emissions:

- Engines
 - o VOC emissions based off manufacture's information. Total facility emissions are below the PSD threshold and, therefore, no limits are being requested.
- Produced Water Tanks
 - The produced water tanks at this station collect minimal condensate volumes.
 The VOC emissions from each tank are estimated based on process model to less than 6tpy.
 - o Recordkeeping
 - Shall maintain records and information adequate to demonstrate its compliance with the requirements of this permit for five years.
- Pneumatic Controllers
 - o Permit Limit:
 - All pneumatic controllers shall be "low bleed" controllers.

Appendix E

Emission Summary

Facility: Bitter Creek Compressor Station

Location: Section 19 T10S R22E

| | Uncontrolled Emissions (TPY) | | | | | | | | | | |
|---------|------------------------------|--------|--------|--------|------|---------|------|--------------|---------|----------|----------|
| Unit ID | Description | NOx | CO | VOC | PM10 | CO2e | CH2O | Acetaldehyde | Benzene | Acrolein | HAPS TOT |
| BTC 1 | G3516TALE | 19.4 | 110.0 | 4.3 | 0.0 | 5784.1 | 3.8 | 0.36 | 0.02 | 0.22 | 4.36 |
| BTC 2 | G3516TALE | 19.4 | 110.0 | 4.3 | 0.0 | 5784.1 | 3.8 | 0.36 | 0.02 | 0.22 | 4.36 |
| TK 1-4 | Tank Emissions | - | - | 15.1 | - | 156.4 | - | - | 0.22 | - | 2.23 |
| L-1 | Tank Truck Loading | - | - | Insig. | - | - | _ | - | - | - | - |
| DEHY-1 | Low Emissions TEG Dehy | - | - | 1.0 | - | | - | - | | - | - |
| DEHY-2 | Low Emissions TEG Dehy | - | - | 1.0 | - | | - | - | - | - | - |
| HTR 1 | Line Heater | 0.3 | 0.2 | Insig. | - | 320.3 | - | - | - | - | - |
| HTR 2 | Dehy Reboiler | Insig. | Insig. | Insig. | - | 5.1 | | - | - | - | - |
| HTR 3 | Dehy Reboiler | Insig. | Insig. | Insig. | - | 5.1 | - | - | _ | - | - |
| FUG | Fugitives | - | - | 8.2 | - | - | | - | - | _ | _ |
| | Total | 39.1 | 220.2 | 25.6 | 0.0 | 12044.8 | 7.5 | 0.7 | 0.3 | 0.4 | 10.9 |

| | PTE Emissions (TPY) | | | | | | | | | | |
|---------|------------------------|--------|--------|--------|------|---------|------|--------------|---------|----------|----------|
| Unit ID | Description | NOx | CO | VOC | PM10 | CO2e | CH2O | Acetaldehyde | Benzene | Acrolein | HAPS TOT |
| BTC 1 | G3516TALE | 19.4 | 7.7 | 3.2 | 0.0 | 5784.1 | 0.9 | 0.36 | 0.02 | 0.22 | 1.51 |
| BTC 2 | G3516TALE | 19.4 | 7.7 | 3.2 | 0.0 | 5784.1 | 0.9 | 0.36 | 0.02 | 0.22 | 1.51 |
| TK 1-4 | Tank Emissions | - | - | 15.1 | - | 156.4 | | - | 0.22 | - | 2.23 |
| L-I | Tank Truck Loading | - | - | Insig. | - | - | - | - | - | - | - |
| DEHY-1 | Low Emissions TEG Dehy | - | - | 1.0 | - | _ | - | - | | - | - |
| DEHY-2 | Low Emissions TEG Dehy | - | - | 1.0 | - | - | - | - | - | - | - |
| HTR 1 | Line Heater | 0.3 | 0.2 | Insig. | - | 320.3 | - | - | - | - | - |
| HTR 2 | Dehy Reboiler | Insig. | Insig. | Insig. | - | 5.1 | - | - | - | - | - |
| HTR 3 | Dehy Reboiler | Insig. | Insig. | Insig. | _ | 5.1 | - | | - | - | - |
| FUG | Fugitives | - | - | 8.2 | - | _ | - | - | _ | - | _ |
| | Total | 39.1 | 15.6 | 23.5 | 0.0 | 12044.8 | 1.8 | 0.7 | 0.3 | 0.4 | 5.2 |

Per guidance, PTE accounts for legally and practically enforceable restrictions (emission controls).

Appendix F

Detailed Emission Calculation

Bitter Creek Compressor Station Engine Detail Sheet

| Source ID No | imber BTC 1 | l |
|--------------|-------------|---|
|--------------|-------------|---|

Source Description 4-Cycle Lean Burn
Engine Usage Compressor Engine

Engine Make Caterpillar Potential operation 8760 hr/yr

Engine Model G3516TALE

Serial Number WPW00523 Manufacture Date 11/14/2006

Date in Service 5/17/2007 Potential fuel usage 96.2 MMscf/yr

Emission Controls Lean Burn 10979 scf/hr

Oxidation Catalyst/AFR

Stack ID BTC 1

Engine Rating 1340 BHP Stack Height ft Stack Diameter 1.0 ft Fuel Heating Value 905.0 Btu/scf Heat Rate 9.94 MMBtu/hr Exit Velocity 78.4 ft/s 840 deg F Engine Heat Rate 7415 Btu/hp-hr Exit Temperature Volume Flow Rate 3,690 ft³/min

Uncontrolled Emissions

| Pollutant | Emission Factor | | Estimated Emissions | | Source of Emission Factor | |
|--------------|-----------------|-----------|---------------------|---------------------|---------------------------|--------|
| | (lb/MMBtu) | (g/hp-hr) | (lb/hr) | (tpy) | | |
| NOx | 0.45 | 1.50 | 4.43 | 19.4 | Manuf. Data | _ |
| CO | 2.53 | 8.50 | 25.11 | 110.0 | Manuf. Data | |
| VOC | 0.10 | 0.33 | 0.97 | 4.3 | Manuf. Data | |
| SOx | 5.88E-04 | 0.002 | 0.01 | 0.03 | AP-42, Table 3.2-2 | |
| PM10 | 7.71E-05 | 0.0003 | 0.00 | 0.00 | AP-42, Table 3.2-2 | |
| PM2.5 | 7.71E-05 | 0.0003 | 0.00 | 0.00 | AP-42, Table 3.2-2 | |
| CO2e | 132.9 | 447.0210 | 1320.56 | 5784.07 | GHG Subpart C Calc. | |
| HAPs | | | | | | lb/yr |
| НСНО | 0.09 | 0.29 | 0.86 | 3.75 | Manuf. Data | 7504.8 |
| Benzene | 4.40E-04 | 0.0015 | 0.004 | 0.02 | AP-42, Table 3.2-2 | 38.3 |
| Acrolein | 5.14E-03 | 0.0173 | 0.051 | 0.22 | AP-42, Table 3.2-2 | 447.4 |
| Acetaldehyde | 8.36E-03 | 0.0281 | 0.083 | 0.36 4.36 | AP-42, Table 3.2-2 | 727.7 |

PTE Emissions

| Pollutant | Emission | Emission Factor | | Emissions | Source of Emission Factor | |
|--------------|------------|-----------------|---------|-----------|---------------------------|--------|
| | (lb/MMBtu) | (g/hp-hr) | (lb/hr) | (tpy) | | |
| NOx | 0.45 | 1.50 | 4.43 | 19.4 | Manuf. Data | |
| CO* | 0.18 | 0.60 | 1.76 | 7.7 | Manuf. Control Data | |
| VOC* | 0.07 | 0.25 | 0.73 | 3.2 | Manuf. Data | |
| SOx | 5.88E-04 | 0.002 | 0.01 | 0.03 | AP-42, Table 3.2-2 | |
| PM10 | 7.71E-05 | 0.0003 | 0.00 | 0.00 | AP-42, Table 3.2-2 | |
| PM2.5 | 7.71E-05 | 0.0003 | 0.00 | 0.00 | AP-42, Table 3.2-2 | |
| HAPs | | | | | | |
| HCHO* | 0.02 | 0.07 | 0.21 | 0.90 | Manuf. Control Data | 1801.2 |
| Benzene | 4.40E-04 | 0.0015 | 0.004 | 0.02 | AP-42, Table 3.2-2 | 38.3 |
| Acrolein | 5.14E-03 | 0.0173 | 0.051 | 0.22 | AP-42, Table 3.2-2 | 447.4 |
| Acetaldehyde | 8.36E-03 | 0.0281 | 0.083 | 0.36 | AP-42, Table 3.2-2 | 727.7 |

^{*}CO: 93% Control Efficiency; VOC: 25% Control Efficiency; Formaldehyde: 76% Control Efficiency

Bitter Creek Compressor Station Engine Detail Sheet

| Source ID Number | BTC 2 |
|------------------|-------|
|------------------|-------|

Source Description 4-Cycle Lean Burn Engine Usage Compressor Engine

Engine Make Caterpillar Potential operation 8760 hr/yr

Engine Model G3516TALE

Serial Number WPW00201 Manufacture Date 5/30/2006

Date in Service 10/5/2010 Potential fuel usage 96.2 MMscf/yr 10979 scf/hr

Emission Controls Lean Burn

Oxidation Catalyst/AFR

Stack ID BTC 2

Engine Rating 1340 BHP Stack Height ft 1.0 ft Fuel Heating Value 905.0 Btu/scf Stack Diameter Heat Rate 9.94 MMBtu/hr Exit Velocity 78.4 ft/s 840 deg F Engine Heat Rate 7415 Btu/hp-hr Exit Temperature Volume Flow Rate 3,690 ft³/min

Uncontrolled Emissions

| Pollutant | Emission | ssion Factor Estimated Emissions | | Source of Emission | | |
|--------------|------------|----------------------------------|---------|--------------------|---------------------|--------|
| l | (lb/MMBtu) | (g/hp-hr) | (lb/hr) | (tpy) | Factor | |
| NOx | 0.45 | 1.50 | 4.43 | 19.4 | Manuf. Data | |
| CO | 2.53 | 8.50 | 25.11 | 110.0 | Manuf. Data | |
| VOC | 0.10 | 0.33 | 0.97 | 4.3 | Manuf. Data | |
| SOx | 5.88E-04 | 0.002 | 0.01 | 0.03 | AP-42, Table 3.2-2 | |
| PM10 | 7.71E-05 | 0.0003 | 0.00 | 0.00 | AP-42, Table 3.2-2 | |
| PM2.5 | 7.71E-05 | 0.0003 | 0.00 | 0.00 | AP-42, Table 3.2-2 | |
| CO2e | 132.9 | 447.0 | 1320.6 | 5784.1 | GHG Subpart C Calc. | |
| HAPs | | | | | • | lb/yr |
| НСНО | 0.09 | 0.29 | 0.86 | 3.75 | Manuf. Data | 7504.8 |
| Benzene | 4.40E-04 | 0.0015 | 0.004 | 0.02 | AP-42, Table 3.2-2 | 38.3 |
| Acrolein | 5.14E-03 | 0.0173 | 0.051 | 0.22 | AP-42, Table 3.2-2 | 447.4 |
| Acetaldehyde | 8.36E-03 | 0.0281 | 0.083 | 0.36 | AP-42, Table 3.2-2 | 727.7 |
| - | | | | 4 36 | | |

PTE Emissions

| Pollutant | Emission | Emission Factor | | Emission Factor Estimated Emissions | | Source of Emission |] |
|--------------|------------|-----------------|---------|-------------------------------------|---------------------|--------------------|---|
| | (lb/MMBtu) | (g/hp-hr) | (lb/hr) | (tpy) | Factor | | |
| NOx | 0.45 | 1.50 | 4.43 | 19.4 | Manuf. Data | _ | |
| CO* | 0.18 | 0.60 | 1.76 | 7.7 | Manuf. Control Data | | |
| VOC* | 0.07 | 0.25 | 0.73 | 3.2 | Manuf. Data | | |
| SOx | 5.88E-04 | 0.002 | 0.01 | 0.03 | AP-42, Table 3.2-2 | | |
| PM10 | 7.71E-05 | 0.0003 | 0.00 | 0.00 | AP-42, Table 3.2-2 | | |
| PM2.5 | 7.71E-05 | 0.0003 | 0.00 | 0.00 | AP-42, Table 3.2-2 | | |
| HAPs | | | | | | | |
| HCHO* | 0.02 | 0.07 | 0.21 | 0.90 | Manuf. Control Data | 1801.2 | |
| Benzene | 4.40E-04 | 0.0015 | 0.004 | 0.02 | AP-42, Table 3.2-2 | 38.3 | |
| Acrolein | 5.14E-03 | 0.0173 | 0.051 | 0.22 | AP-42, Table 3.2-2 | 447.4 | |
| Acetaldehyde | 8.36E-03 | 0.0281 | 0.083 | 0.36 | AP-42, Table 3.2-2 | 727.7 | |

^{*}CO: 93% Control Efficiency; VOC: 25% Control Efficiency; Formaldehyde: 76% Control Efficiency



| Names | Units | Flash |
|---------------------------|--------|--------|
| Carbon Dioxide(Mass Flow) | ton/yr | 1 |
| Methane(Mass Flow) | ton/yr | 7.4 |
| Benzene(Mass Flow) | ton/yr | 0.22 |
| Toluene(Mass Flow) | ton/yr | 0.17 |
| Ethylbenzene(Mass Flow) | ton/yr | 0.0069 |
| p-Xylene(Mass Flow) | ton/yr | 0.03 |
| n-Hexane(Mass Flow) | ton/yr | 1.8 |

Annual tank loss calculations for "Mixed Liquids Intet".
Flashing losses are 15.11 tonlyr.
* Only Non-Exempt VOC are reported.

Tank-



| Names | Units | Mitted Liquids Intel | Flash | Mitted Liquids to Truck |
|-------------------------------|-------|----------------------|--------|-------------------------|
| Carbon Dioxide(Mole Fraction) | % | 0.0073 | 2.7 | 0.0015 |
| Nitrogen(Mole Fraction) | % | 7.7e-05 | 0.036 | 5e-07 |
| Methane(Mole Fraction) | % | 0.12 | 54 | 0.0024 |
| Elhane(Mole Fraction) | % | 0.025 | 11 | 0.0021 |
| Propane(Mole Fraction) | % | 0.028 | 10 | 0.0054 |
| I-Eutane(Mole Fraction) | % | 0.013 | 3.5 | 0.0058 |
| n-Butzne(Mole Fraction) | % | 0.026 | 5.7 | 0.014 |
| I-Pertane(Mole Fraction) | % | 0.024 | 2.8 | 0.018 |
| n-Perlane(Mole Fraction) | % | 0.028 | 2.5 | 0.022 |
| Heptane(Mole Fraction) | % | 0.1 | 0.9 | 0.1 |
| n-Octane(Mote Fraction) | % | 0.063 | 0.21 | 0.063 |
| Nonane(Mote Fraction) | % | 0.013 | 0.0094 | 0.013 |
| C10+(Mole Fraction) | % | | | |
| Benzene(Mote Fraction) | % | 0.014 | 0.33 | 0.013 |
| Toluene(Mote Fraction) | % | 0.028 | 0.21 | 0.028 |
| Elly@enzene(Mole Fraction) | % | 0.0033 | 0.0075 | 0.0033 |
| p-Xylene(Mole Fraction) | % | 0.014 | 0.033 | 0.014 |
| n-Heame(Mote Fraction) | % | 0.088 | 2.4 | 0.083 |
| Liquid Volumeiric Flow | bbld | 157.92 | 395.08 | 118.47 |

Annual tank loss calculations for "Mixed Liquids Inlet".

Total working and breathing losses from the Vertical Cylinder are 0.01289 ton/yr.

Loading losses are 0.01476 ton/yr of loaded liquid.

* Only Non-Exempt VOC are reported.

Tank

Bitter Creek Compressor Station Annual Condensate Throughput

| | | Condensate | Average | Water | Average | Combined | Average |
|------|---------|------------------|------------|------------|------------|------------|------------|
| | | Production | Production | Production | Production | Production | Production |
| Year | Month | bbls/month | bbls/day | bbls/month | bbls/day | bbls/month | bbls/day |
| | Jan | 0 | 0 | 1440 | 46 | 1440 | 48.0 |
| | Feb | 40 | 1 | 2180 | 70 | 2220 | 74.0 |
| | Mar | 450 | 15 | 2100 | 68 | 2550 | 85.0 |
| | Apr | 180 | 6 | 2860 | 92 | 3040 | 101.3 |
| | May | 370 | 12 | 2810 | 91 | 3180 | 106.0 |
| 2014 | Jun | 40 | 1 | 1320 | 43 | 1360 | 45.3 |
| 2014 | Jul | 0 | 0 | 1930 | 62 | 1930 | 64.3 |
| | Aug | 0 | 0 | 1745 | 56 | 1745 | 58.2 |
| | Sep | 0 | 0 | 2090 | 67 | 2090 | 69.7 |
| | Oct | 40 | 1 | 2730 | 88 | 2770 | 92.3 |
| | Nov | 0 | 0 | 2490 | 80 | 2490 | 83.0 |
| | Dec | 120 | 4 | 2290 | 74 | 2410 | 80.3 |
| | Jan | 40 | 1 | 1080 | 35 | 1120 | 37.3 |
| | Feb | 140 | 5 | 2180 | 70 | 2320 | 77.3 |
| | Mar | 120 | 4 | 1070 | 35 | 1190 | 39.7 |
| | Apr | 0 | 0 | 1760 | 57 | 1760 | 58.7 |
| | May | 160 | 5 | 2510 | 81 | 2670 | 89.0 |
| 2015 | Jun | 0 | 0 | 890 | 29 | 890 | 29.7 |
| 2015 | Jul | 0 | 0 | 3555 | 115 | 3555 | 118.5 |
| | Aug | 0 | 0 | 960 | 31 | 960 | 32.0 |
| | Sep | 0 | 0 | 480 | 15 | 480 | 16.0 |
| | Oct | 0 | 0 | 690 | 22 | 690 | 23.0 |
| | Nov | 0 | 0 | 640 | 21 | 640 | 21.3 |
| | Dec | 0 | 0 | 1670 | 54 | 1670 | 55.7 |
| - | Average | Daily Production | 2 | | 63 | | 68 |

Max 2015 Avg Daily Production

118.5

Bitter Creek Compressor Station Heater Emission Calculation Sheet

Insignificant Source

| Heater Data | | | |
|-------------------|-------------|--|--|
| ID | HTR 1 | | |
| Description | Line Heater | | |
| Nameplate Rating: | 0.50 | (MMBtu/hr) | |
| Efficiency: | 0.80 | (decimal) | |
| Heat Input: | 0.63 | (MMBtu/hr) | |
| Operation: | 8760 | (hr/yr) | |
| Fuel Heat Value: | 1200.0 | (Btu/scf) | |
| VOC Wt Fraction: | 0.07 | (decimal, VOC weight fraction of the fuel gas) | |

| Emission Factors | | | | | |
|---------------------|--------|-------|-------|-------------------|--|
| | NO_X | CO | TOC | CH ₂ O | |
| lb/MMscf | 100 | 84 | 11 | 0.075 | |
| Adjusted lb/MMscf * | 117.6 | 87.7 | 12.9 | 0.09 | |
| lb/MMBtu | 0.115 | 0.086 | 0.013 | 0.000 | |

^{*} Emission factor conversion based on footnote "a" of AP-42 Table 1.4-1 to convert from 1,020 Btu/scf to the above Fuel Heat Value in units of Btu/scf.

| NO | X | (| 0 | V(| OC | CH | I ₂ O |
|---------|----------|---------|----------|---------|----------|---------|------------------|
| (lb/hr) | (ton/yr) | (lb/hr) | (ton/yr) | (lb/hr) | (ton/yr) | (lb/hr) | (ton/yr) |
| 0.07 | 0.32 | 0.05 | 0.24 | 0.00 | 0.00 | 0.00 | 0.00 |

| Conversions: | | | |
|------------------|-----------|--------------------|--------|
| 1 Metric Ton | = 2204.62 | lbs | |
| 1 kg | = 0.001 | metric tons | |
| Pollutant | kg/mmbtu | metric ton | tpy |
| CO ₂ | 53.02 | 290 | 319.98 |
| CH₄ | 0.001 | 0.0 | 0.01 |
| N ₂ O | 0.0001 | 0.0 | 0.00 |
| | • | CO _{2e} = | 320 |

Bitter Creek Compressor Station Heater Emission Calculation Sheet Insignificant Source

| ID | HTR-2 | HTR-3 | |
|-------------------|----------------|--|--|
| Description | Deliy Reboiler | | |
| Nameplate Rating: | 0.01 | (MMBtu/hr) | |
| Efficiency: | 0.80 | (decimal) | |
| Heat Input: | 0.01 | (MMBtu/hr) | |
| Operation: | 8760 | (hr/yr) | |
| Fuel Heat Value: | 1200.0 | (Btu/scf) | |
| VOC Wt Fraction: | 0.07 | (decimal, VOC weight fraction of the fuel gas) | |

| Emission Factors | | | | | |
|---------------------|--------|-------|-------|-------------------|------|
| | NO_X | CO | TOC | CH ₂ O | |
| lb/MMscf | 100 | 84 | 11 | 0.075 | |
| Adjusted lb/MMscf * | 117.6 | 87.7 | 12.9 | 0.09 | |
| lb/MMBtu | 0.115 | 0.086 | 0.013 | 0.000 | |

^{*} Emission factor conversion based on footnote "a" of AP-42 Table 1.4-1 to convert from 1,020 Btu/scf to the above Fuel Heat Value in units of Btu/scf.

| NO _X | | CO | | VOC | | CH ₂ O | |
|-----------------|----------|---------|----------|---------|----------|-------------------|----------|
| (lb/hr) | (ton/yr) | (lb/hr) | (ton/yr) | (lb/hr) | (ton/yr) | (lb/hr) | (ton/yr) |
| 0.00 | 0.01 | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 | 0.00 |

| Conversions: | | | |
|------------------|----------|--------------------|------|
| 1 Metric Ton = | 2204.62 | lbs | |
| 1 kg = | 0.001 | metric tons | |
| Pollutant | kg/mmbtu | metric ton | tpy |
| CO ₂ | 53.02 | 5 | 5.12 |
| CH ₄ | 0.001 | 0.0 | 0.00 |
| N ₂ O | 0.0001 | 0.0 | 0.00 |
| | <u> </u> | CO _{2e} = | 5 |

Bitter Creek Compressor Station Fugitives Detail Sheet

Component Source Counts for Gas Plant/Compressor Station Units

| - Composition Comp | | | | | | | | | |
|--|------------|-----------|-----------------|----------|----------|----------------|--------------|----------------------|-------|
| Equipment Type | Compressor | Separator | Condensate Tank | TEG Unit | DEA Unit | C3 Refrig Skid | Expan Demeth | Mole Sieve System | Flare |
| For this facility, Number of Units | 6 | 6 | 3 | 2 | 0 | 0 | 0 | 0 | 0 |
| Valves - Inlet Gas | 40 | 6 | 4 | 75 | 15 | 40 | 40 | 25 | 8 |
| Valves - Liquid | 5 | 4 | 6 | 20 | 60 | 35 | 35 | 0 | |
| Relief Valves | 2 | 2 | 2 | 4 | 4 | 6 | 6 | 4 | 2 |
| Pump Seals - Liquid | 0 | 0 | 2 | 4 | 4 | 0 | 0 | 0 | 0 |
| Flanges/Connectors - Inlet Gas | 150 | 50 | 50 | 250 | 250 | 250 | 250 | 100 | 75 |
| Flanges/Connectors - Liquid | 10 | 10 | 10 | 20 | 20 | 20 | 20 | 20 | 10 |
| Compressor Seals | 4 | 0 | 0 | 0 | 0 | 6 | 0 | 0 | 0 |

| | o | | | |
|--|---|--|--|--|
| | | | | |
| | | | | |

| | | ugitives | | | | | | |
|--------------------------------|-----------------------------------|---------------|-----------|--------|------------------------------|------------------------------|----------------------------|----------------------------|
| Equipment Type | Emission Factor (lb/hr/source) | Source Count* | % VOC C3+ | %HAP | VOC Emission Rate (lb/hr) | HAP Emission Rate (lb/hr) | HAP Emission Rate (tpy) | VOC Emission Rate (tpy) |
| Valves - Inlet Gas | 0.00992 | 438 | 11.40% | 0.12% | 0.495 | 0.005 | 0.023 | 2.17 |
| Valves - Liquid | 0.00550 | 112 | 100.00% | 11.40% | 0.616 | 0.070 | 0.308 | 2.70 |
| Relief Valves | 0.01940 | 38 | 11.40% | 0.12% | 0.084 | 0.001 | 0.004 | 0.37 |
| Pump Seals - Liquid | 0.02866 | 14 | 100.00% | 11.40% | 0.401 | 0.046 | 0.200 | 1.76 |
| Flanges/Connectors - Inlet Gas | 0.00086 | 1850 | 11.40% | 0.12% | 0.181 | 0.002 | 0.008 | 0.79 |
| Flanges/Connectors - Liquid | 0.00024 | 190 | 100.00% | 11.40% | 0.046 | 0.005 | 0.023 | 0.20 |
| Compressor Seals | 0.01940 | 24 | 11.40% | 0.12% | 0.053 | 0.001 | 0.002 | 0.23 |
| Total | | | | | 1.877 | 0.130 | 0.57 | 8.22 |

Source counts estimated from similar facilities. These counts are not actuals.

Source EPA Protocol for Equipment Leak Emission Estimates, November, 1995, EPA-453/R-95-017

Appendix G

Regulatory Analysis

Regulatory Analysis

40 CFR 60 - New Source Performance Standards (NSPS)

<u>Subpart A: General Provisions.</u> This subpart applies to the owner or operator of any stationary source which contains an affected facility, the construction or modification of which is commenced after the date of publication of any standard in part 60. The general provisions under subpart A apply to sources that are subject to the specific subparts of part 60. This facility is not subject to specific subparts of part 60; therefore, the General Provisions of part 60 do not apply.

<u>Subpart Dc</u> Standards of Performance for Small Industrial, Commercial, Institutional Steam Generating Units, applies to steam generating units having a capacity between 10 MMBtu/hr and 100 MMBtu/hr that are constructed or modified after June 9, 1989. There are no emission units that meet the definition of a steam generating unit at this facility. Therefore, the requirements of subpart Dc do not apply.

<u>Subpart Kb</u> Standards of Performance for Volatile Organic Liquid Storage Vessels, applies to each storage vessel with a capacity greater than or equal to 75 cubic meters used to store volatile organic liquids (VOL) for which construction, reconstruction, or modification is commenced after July 23, 1984. There are no storage tanks greater than 75 cubic meters that store volatile organic liquids at this facility which vent emissions to the atmosphere, therefore Subpart Kb does not apply.

<u>Subpart KKK</u> Standards of Performance for Equipment Leaks of VOC from Onshore Natural Gas Processing Plants apply to affected facilities in onshore natural gas processing plants that commenced construction, modification or reconstruction after January 20, 1984. A natural gas processing plant is defined in the Subpart as any site "engaged in the extraction of natural gas liquids from field gas". This facility does not contain processes which extract natural gas liquids from field gas. Therefore, this rule does apply.

<u>Subpart LLL</u> Standards of Performance for Onshore Natural Gas Processing; SO2 Emissions. This rule applies to sweetening units and sulfur recovery units at onshore natural gas processing facilities. This facility is not an onshore natural gas processing facility. Therefore, this rule does not apply.

<u>Subpart IIII</u> Standards of Performance for Stationary Compression Ignition Internal Combustion Engines applies to manufacturers, owners and operators of stationary compression ignition (CI) internal combustion engines (ICE). There are no stationary compression ignition engines at this site, therefore Subpart IIII does not apply.

<u>Subpart JJJJ</u> Standards of Performance for Stationary Spark Ignition Internal Combustion Engines applies to manufacturers, owners and operators of stationary spark ignition (SI) internal combustion engines (ICE). This applies to engines that were ordered from the manufacturer after June 12, 2006 and;

- Are greater than 500 hp and manufactured after July 1, 2007 or
- Lean burn engines greater than 500 hp but less than 1,350 hp and manufactured after January 1, 2008

Engines BTC 1 and BTC 2 are lean burn engines greater than 500 hp but less than 1,350 hp that were manufactured prior to January 1, 2008; therefore, subpart JJJJ does not apply to these engines.

<u>Subpart OOOO</u> Standards of Performance for Crude Oil and Natural Gas Production, Transmission and Distribution. This subpart establishes emissions standards and compliance schedules for the control of VOCs and SO2 emissions from affected facilities that commenced construction, modification or reconstruction after August 23, 2011. The rule applies to equipment leaks at onshore natural gas processing plants and compressors. This facility is not a natural gas processing plant and compressors were constructed prior to August 23, 2011; therefore, subpart OOOO is not applicable.

40 CFR 61 - National Emission Standards for Hazardous Air Pollutants

<u>Subpart V</u> National Emission Standard for Equipment Leaks (Fugitive Emission Sources). This subpart applies to sources that are intended to operate in volatile hazardous air pollutant (VHAP) service. Based on engineering judgment, historical and recent gas composition and facility process it can be predicted that the percent VHAP content will never exceed 10 percent by weight; therefore Subpart V is not an applicable regulation for the facility.

40 CFR 63 - National Emission Standards for Hazardous Air Pollutants (NESHAP)

<u>Subpart HH</u> National Emission Standards for Hazardous Air Pollutants from Oil and Natural Gas Production Facilities, applies to glycol dehydration units, storage vessels with potential for flash emissions, and ancillary equipment operating in volatile hazardous air pollutant service that is located at a natural gas processing plant which is a major source of HAPS. This facility is not a natural gas processing plant therefore Subpart HH does not apply.

<u>Subpart HHH</u> National Emission Standards for Hazardous Air Pollutants from Natural Gas Transmission and Storage Facilities. This rule applies to natural gas transmission and storage facilities that transport or store natural gas prior to entering the pipeline to a local distribution company or to a final end user, and that are a major source of HAP emissions. This subpart does not apply to this facility because it does not meet the definition of a Natural Gas Transmission and Storage Facility

<u>Subpart EEEE</u> National Emission Standards for Hazardous Air Pollutants: Organic Liquids Distribution (Non-Gasoline). This rule establishes national emission limitations, operating limits, and work practice standards for organic HAPs emitted from organic liquids distribution operations at major sources of HAP emissions. In this subpart, organic liquids distribution operations do not include oil and natural gas production field facilities as defined in subpart HH or natural gas transmission and storage facilities as defined in subpart HHH. This facility meets the definition an oil and natural gas production field facility as defined in §63.761 of subpart HH. Therefore, this rule does not apply.

<u>Subpart ZZZZ</u> National Emission Standards for Hazardous Air Pollutants for Stationary Reciprocating Internal Combustion Engines (RICE) establishes national emission limitations and operating limitations for HAPs emitted from stationary reciprocating internal combustion engines, and requirements to demonstrate initial and continuous compliance with the emission limitations and operating limitations. This facility is an area source of HAPs; therefore, the facility is not subject to major source ZZZZ requirements. All engines (emission units BTC 1 through BTC 2) at the facility are subject to the August 20, 2010 revisions to MACT ZZZZ for existing units at areas sources of HAPs. This facility is by definition a remote sources and will comply with applicable requirements of this regulation.

40 CFR 98 - Green House Gas Reporting

Subpart A, General Provisions applies to a facility that contains any source category (as defined in subparts C through JJ of this part) that is listed in this paragraph (a)(2) in any calendar year starting in 2010 and that emits 25,000 metric tons CO2e or more per year in combined emissions from stationary fuel combustion units, miscellaneous uses of carbonate, and all source categories that are listed in this regulation. The facility is subject to the reporting requirements of Subpart C and Subpart W.